

## Extended Hildebrand Solubility Approach applied to Nimodipine in PEG 400 + ethanol mixtures

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### SUMMARY

Nimodipine (NMD) is a drug used as cerebral vasodilator whose physicochemical properties in solution have not been studied completely. In this work the Extended Hildebrand Solubility Approach (EHSA) was applied to evaluate the equilibrium solubility of NMD in some polyethylene glycol 400 + ethanol mixtures at 298.15 K. An acceptable correlative capacity of EHSA was found using a regular polynomial model in order three (overall deviation lower than 1.3%), when the  $W$  interaction parameter is related to the solubility parameter of the mixtures. Moreover, the mean deviation obtained in the estimated solubility with respect to experimental solubility was lower than the one obtained directly by means of an empiric regression in order three of the logarithm experimental solubility as a function of the mixtures' solubility parameters (1.7%).

*Key words:* Nimodipine, PEG 400 + ethanol, Extended Hildebrand Solubility Approach, binary mixtures, solubility parameter.

## RESUMEN

### Método extendido de Hildebrand aplicado a la solubilidad de nimodipina en mezclas PEG 400 + etanol

La nimodipina (NMD) es un agente usado como vasodilatador cerebral y cuyas propiedades fisicoquímicas en solución aún no han sido totalmente estudiadas. En la presente investigación se aplicó el Método Extendido de Solubilidad de Hildebrand (MESH) al estudio de la solubilidad de NMD en algunas mezclas binarias PEG 400 + etanol a 298,15 K. Se obtuvo una capacidad predictiva aceptable del MESH (desviación general inferior al 1,3%) al utilizar un modelo polinómico regular de tercer orden, relacionando el parámetro de interacción  $W$  con el parámetro de solubilidad de las mezclas solventes. De esta forma, las desviaciones obtenidas en la solubilidad estimada fueron de magnitud inferior a las obtenidas al calcular esta propiedad directamente, utilizando una regresión empírica regular del mismo orden, de la solubilidad experimental del fármaco en función del parámetro de solubilidad de las mezclas disolventes, en la cual se obtuvo una desviación promedio del 1,7%.

*Palabras clave:* nimodipina, PEG 400 + etanol, Método Extendido de Solubilidad de Hildebrand, mezclas binarias, parámetro de solubilidad.

## INTRODUCTION

Nimodipine (NMD, Figure 1, molar mass  $418.44 \text{ g mol}^{-1}$ ) is a calcium channel blocker that prevents the calcium-dependent smooth muscle contraction and therefore, the subsequent vasoconstriction. NMD exhibits greater effects on cerebral circulation than on peripheral circulation, and for this reason, it is specially used as an adjunct to improve the neurologic outcome following subarachnoid hemorrhage from ruptured intracranial aneurysm [1].

On the other hand, NMD aqueous solubility is too low to allow the design of homogeneous liquid dosage forms with solvents strictly aqueous [2]. For this reason some disperse and coarse dosage systems have been investigated and developed, which include liposomes [3], solid dispersions [4, 5], cyclodextrin inclusion complexes [6-8], hydrogels and hydrophilic matrices [9, 10], and some emulsions [11]. Nevertheless, in every one of these formulations this drug is dispersed only in a coarse way instead of a molecular one as a real solution. In the Colombian market this drug is presented as tablets, injectable and soft gelatin capsules [12].

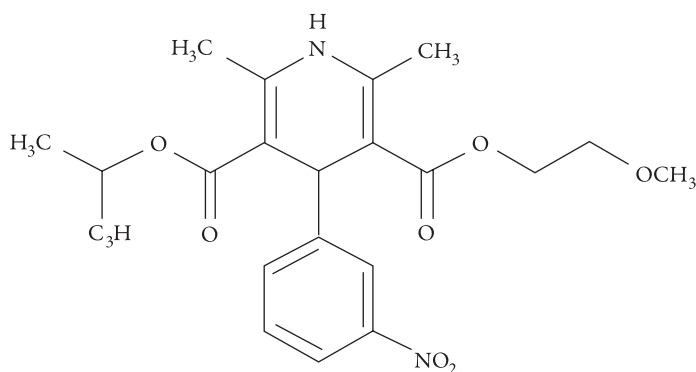


Figure 1. Molecular structure of nimodipine.

Although NMD is used in therapeutics, the physicochemical information about its solubility is not abundant. In this way, it is important to note that cosolvency is the best technique used in pharmacy for increasing drugs solubility to develop homogeneous liquid dosage forms [13]. On the other hand, it is clear that predictive methods of physicochemical properties of drugs are very important for industrial pharmacists because they allow optimizing design processes [14].

For this reason, this work presents a physicochemical study about the solubility prediction of NMD in binary mixtures conformed by polyethylene glycol 400 (PEG 400) and ethanol. The study was done based on the Extended Hildebrand Solubility Approach (EHSA) [15]. Up to the best of our knowledge no report about the application of EHSA method to this drug has been presented in the literature. It is relevant to keep in mind that EHSA method has been widely used to study the solubility of a lot of pharmaceutical compounds [16-38]. On the other hand, PEG 400 is, after ethanol and propylene glycol, the cosolvent more employed to develop liquid pharmaceutical dosage forms [39]. Moreover, PEG 400 is also employed to regulate the evaporation in liquid products [40].

## THEORETICAL

The real solubility ( $X_2$ ) of a solid solute in a liquid solution is calculated adequately by means of the expression,

$$-\log X_2 = \frac{\Delta H_{fus} (T_{fus} - T)}{2.303RT_{fus}T} + \log \gamma_2 \quad (\text{Eq. 1})$$

where,  $\Delta H_{fus}$  is the fusion enthalpy of the solute,  $R$  is the gas constant,  $T_{fus}$  is the melting point of the solute,  $T$  is the absolute temperature of the solution, and  $\log \gamma_2$  is the non-ideality term. It is important to keep in mind that ideal solubility is calculated by means of Equation 1 without consider the second term of the right side. The  $\gamma_2$  term is the activity coefficient of the solute determined experimentally. One method of calculating  $\gamma_2$  is the referent to regular solutions obtained from,

$$-\log X_2 = \frac{\Delta H_{fus} (T_{fus} - T)}{2.303RT_{fus}T} + \frac{V_2\phi_1^2}{2.303RT}(\delta_1 - \delta_2)^2 \quad (\text{Eq. 2})$$

where,  $V_2$  is the partial molar volume of the solute,  $\phi_1$  is the volume fraction of the solvent in the saturated solution, and  $\delta_1$  and  $\delta_2$  are the solubility parameters of solvent and solute, respectively. Pharmaceutical dissolutions deviate of predicted by the regular solutions theory. On this way, Martin *et al.* developed the EHSA method (16-22). If the  $A$  term (defined as  $V_2\phi_1^2 / (2.303RT)$ ) is introduced in the equation 3, the real solubility of drugs can be calculated from the expression,

$$-\log X_2 = -\log X_2^{id} + A(\delta_1^2 + \delta_2^2 - 2W) \quad (\text{Eq. 3})$$

where, the  $W$  term is equal to  $2K\delta_1\delta_2$  (where,  $K$  is the Walker parameter). The  $W$  factor can be calculated from experimental data by means of,

$$W = 0.5 \times \left( \delta_1^2 + \delta_2^2 - \frac{\log \gamma_2}{A} \right) \quad (\text{Eq. 4})$$

where,  $\gamma_2$  is the activity coefficient of the solute in the saturated solution, and it is calculated as,  $X_2^{id} / X_2$ . The experimental values of the  $W$  parameter can be correlated by means of regression analysis by using regular polynomials as a function of  $\delta_1$ , as follows,

$$W = C_0 + C_1\delta_1 + C_2\delta_1^2 + C_3\delta_1^3 \dots + C_n\delta_1^n \quad (\text{Eq. 5})$$

These empiric models can be used to estimate the drug solubility by means of back-calculation resolving this property from the specific  $W$  value obtained in the respective polynomial regression. A lot of examples of the application of the previous equations have been reported in the literature [15-38].

## EXPERIMENTAL

### Reagents

Nimodipine (1,4-dihydro-2,6-dimethyl-4-(3-nitrophenyl)-3,5-pyridinedicarboxylic acid 2-methoxyethyl 1-methylethyl ester; CAS No. 66085-59-4; Haohua Ind. & Co., China), polyethylene glycol 400 (Dow Chemical Co., USA), and absolute ethanol A.R. (Merck, Germany), used in this research, were in agreement with the quality requirements of the American Pharmacopeia, USP [41].

### Solvent mixtures preparation

Both solvents were dried by using molecular sieve (Merck, 3 Å) before preparing the mixtures. All PEG 400 + ethanol mixtures were prepared by mass, using an Ohaus Pioneer TM PA214 analytical balance with sensitivity of  $\pm 0.1$  mg, in quantities of 50 g. The mass fractions of PEG 400 of the nine binary mixtures prepared varied by 0.10 from 0.10 to 0.90.

### Solubility determinations

An excess of NMD was added to approximately 10 g of each solvent mixture or neat solvents, in stoppered dark glass flasks. The flasks with the solid-liquid mixtures were placed in re-circulating thermostatic baths (Neslab RTE 10 Digital One Thermo Electron Company) kept at  $298.15 \pm 0.05$  K for at least 7 days to reach the equilibrium. After this time the supernatant solutions were filtered at isothermal conditions (Millipore Corp. Swinnex<sup>®</sup>-13) to ensure that they were free of particulate matter before sampling for composition analysis. NMD concentrations were determined by UV-spectrophotometric analysis at 236 nm after alcoholic dilution. All the solubility experiments were run at least in triplicates. In order to transform mole fractions to molar concentrations ( $\text{mol dm}^{-3}$ ), the density of the saturated solutions was determined with a digital density meter (DMA 45 Anton Paar) connected to the same re-circulating thermostatic baths [42].

### Calorimetric study

Melting point and enthalpy of fusion of NMD were determined by DSC studies (DSC 823E Mettler Toledo). Thermal analyses were performed at a heating rate of  $10 \text{ K min}^{-1}$  in a dynamic nitrogen atmosphere ( $60 \text{ cm}^3 \text{ min}^{-1}$ ). Nearly 1.5 mg of drug was used. The equipment was calibrated using Indium as standard [43].

### Estimation of the volumetric contributions

Apparent specific volume ( $\phi_V^{\text{spc}}$ ) were calculated according to equation 6, where,  $m_2$  and  $m_1$  are the masses of solute and solvent in the saturated solution, respectively,  $VE_1$  is the specific volume of the solvent, and  $\rho_{\text{soln}}$  is the solution density [44].

$$\phi_V^{\text{spc}} = \frac{m_2 + m_1(1 - VE_1\rho_{\text{soln}})}{m_2\rho_{\text{soln}}} \quad (\text{Eq. 6})$$

The NMD apparent molar volume is calculated by multiplying the  $\phi_V^{\text{spc}}$  value and the molar mass of the solute.

## RESULTS AND DISCUSSION

The information about polarity and volumetric behavior of PEG 400 + ethanol mixtures as a function of the composition is shown in Table 1 [45]. On the other hand, the calorimetric values of fusion for NMD were as follows,  $T_{\text{fus}} = 397.2$  K and  $\Delta H_{\text{fus}} = 41.68$  kJ mol<sup>-1</sup>. From these values the calculated ideal solubility for this drug calculated by using Equation 7 was  $1.513 \times 10^{-2}$  in mole fraction.

$$-\log X_2^{\text{id}} = \frac{\Delta H_{\text{fus}}(T_{\text{fus}} - T)}{2.303RT_{\text{fus}}T} \quad (\text{Eq. 7})$$

Table 1 also summarizes the NMD solubility expressed in molarity and mole fraction, the density of the saturated mixtures, the apparent molar volume of NMD, and the solvent volume fraction in the saturated solutions at 298.15 K. It is interesting to note that when molarity is considered the maximum drug solubility is obtained in the mixture with  $\delta_1 = 24.00$  MPa<sup>1/2</sup> (0.7367 in volume fraction of PEG 400) but if the mole fraction scale is considered the maximum is obtained in neat PEG 400 (with  $\delta_1 = 23.10$  MPa<sup>1/2</sup>). This result is a consequence of the definition of each concentration scale [15]. Nevertheless, in this case the useful scale is mole fraction.

From density values of cosolvent mixtures and saturated solutions, in addition to NMD solubility, the solvent volume fraction ( $\phi_1$ ) and apparent molar volume of the solute ( $\phi_V^{\text{mol}}$ ) in the saturated mixtures, were calculated. These values are also presented in Table 1.

Table 1. PEG 400 + ethanol solvent mixtures composition, Hildebrand solubility parameter of mixtures, nimodipine solubility expressed in molarity and in mole fraction, density of the solvents and saturated mixtures, apparent molar volume of nimodipine, solvent volume fraction in the saturated solutions, and activity coefficient of nimodipine as decimal logarithm, at 298.15 K.

$\phi_{\text{PEG}}$	$\delta_1^a / \text{MPa}^{1/2}$	NMD			$\rho_{\text{sol}}^c / \text{g cm}^{-3}$	$\rho_{\text{satd soln}} / \text{g cm}^{-3}$	$\Phi_V^{\text{mol}} / \text{cm}^3 \text{mol}^{-1}$	$\phi_1$	$\log \gamma_2$
		$\text{mol dm}^{-3}$	$X_2$	%VC <sup>b</sup>					
0.0000	26.50	0.115	6.93 E-3	1.51	0.7853	0.8067	295.6	0.9660	0.339
0.0721	26.25	0.133	8.58 E-3	2.61	0.8148	0.8322	353.0	0.9530	0.246
0.1489	25.99	0.162	1.12 E-2	0.98	0.8438	0.8624	359.2	0.9420	0.129
0.2307	25.72	0.193	1.47 E-2	2.30	0.8726	0.8930	358.4	0.9309	0.014
0.3181	25.42	0.225	1.89 E-2	1.19	0.9041	0.9255	357.5	0.9196	-0.097
0.4116	25.10	0.245	2.31 E-2	0.10	0.9360	0.9610	338.4	0.9169	-0.183
0.5121	24.76	0.255	2.77 E-2	2.40	0.9693	0.9883	355.1	0.9093	-0.262
0.6201	24.39	0.279	3.59 E-2	1.93	1.0044	1.0236	348.1	0.9030	-0.375
0.7367	24.00	0.289	4.64 E-2	2.07	1.0419	1.0569	351.8	0.8984	-0.487
0.8630	23.57	0.284	6.19 E-2	1.69	1.0815	1.0915	354.2	0.8994	-0.612
1.0000	23.10	0.267	9.52 E-2	1.87	1.1224	1.1282	353.6	0.9055	-0.799

<sup>a</sup>  $\delta_1$  values were calculated additively according to  $\delta_1 = \phi_{\text{PEG}} \delta_{\text{PEG}} + (1 - \phi_{\text{PEG}}) \delta_{\text{EtOH}}$ , where  $\phi_{\text{PEG}}$  is the volume fraction of PEG 400 and  $\delta_{\text{PEG}}$  and  $\delta_{\text{EtOH}}$  are the Hildebrand solubility parameters of PEG 400 (23.1 MPa<sup>1/2</sup>) and ethanol (26.5 MPa<sup>1/2</sup>), respectively [14].

<sup>b</sup> %VC is the percentage variation coefficient of solubility values.

<sup>c</sup> Data from Rodríguez *et al.* [44].

Ultimately, the activity coefficients of NMD as decimal logarithms are also presented in Table 1. These values were calculated from experimental solubility values and ideal solubility at 298.15 K ( $X_2 = 1.513 \times 10^{-2}$ ). In the vast majority of cases,  $\gamma_2$  values were lower than unit (negative logarithmic values) because in those systems (PEG 400-rich mixtures) the experimental solubilities are greater than the ideal one.

Because the maximum mole fraction solubility of NMD was obtained in neat PEG 400 instead of a mixture Table 2 summarizes the results of the application of the group contribution method of Fedors for estimate interne energy, molar volume, and total Hildebrand solubility parameter of nimodipine,  $\delta_{\text{total}} = 21.89 \text{ MPa}^{1/2}$  [46]. According to this result, it is clear that this drug is less polar than PEG 400, which is the less polar solvent employed in this study.

Figure 2 shows the experimental drug solubility and the calculated solubility by using the regular solutions model (Equation 2) as a function of the solubility parameter of solvent mixtures. It is interesting to note that the experimental solubility is greater than the calculated solubility by using the regular solution model in every one of the mixtures evaluated. This result could be attributed to the fact that this semiempirical model does not consider specific interactions between solvent and solute, and all the involved compounds present polar groups that could interact by hydrogen bonding. In particular PEG 400 could interact as Lewis base due to its ether oxygen atoms with the amine groups of NMD (Figure 1). Moreover, other possible interactions between ethanol and this drug could be present due to their carboxyl and nitro groups (Figure 1).

Table 2. Application of the group contribution method of Fedors for estimate interne energy, molar volume, and total Hildebrand solubility parameter of nimodipine.

Group or atom	Quantity	$\Delta U / \text{kJ mol}^{-1}$	$V / \text{cm}^3 \text{mol}^{-1}$
$-\text{CH}_3$	5	$5 \times 4.71 = 23.54$	$5 \times 33.5 = 167.5$
$-\text{CH}_2-$	2	$2 \times 4.94 = 9.87$	$2 \times 16.1 = 32.2$
$>\text{CH}-$	2	$2 \times 3.43 = 6.86$	$2 \times -1.0 = -2.0$
$>\text{C}=\text{}$	4	$4 \times 4.31 = 17.24$	$4 \times -5.5 = -22.0$
Phenylene (m)	1	31.92	52.4
$-\text{COO}-$	2	$2 \times 17.99 = 35.98$	$2 \times 18.0 = 36.0$
$-\text{O}-$	1	3.35	3.8
$-\text{NH}-$	1	8.37	4.5
$-\text{NO}_2$	1	15.36	32.0
Ring closure	1	1.05	16.0
		$\Delta U_{\text{total}} = 153.54$	$V_{\text{total}} = 320.4$
		$\delta_{\text{total}} = (153,540/320.4)^{1/2} = 21.89 \text{ MPa}^{1/2}$	

In order to calculate the  $W$  parameter the calculated  $\delta_{\text{total}}$  value ( $21.89 \text{ MPa}^{1/2}$ , Table 2) was used [46]. On the other hand, the parameters  $A$ ,  $K$ , and  $W$  are presented in Table 3. Figure 3 shows that the variation of the  $W$  parameter with respect to the solubility parameter of solvent mixtures, presents deviation from linear behavior, just as it is expectable because the  $W$  term implies the summation of two quadratic terms ( $\delta_1^2$  and  $\delta_2^2$ ) and one non-constant-quotient involving a logarithmic term ( $-\log \gamma_2 / A$ ) as it is shown in Equation 4.



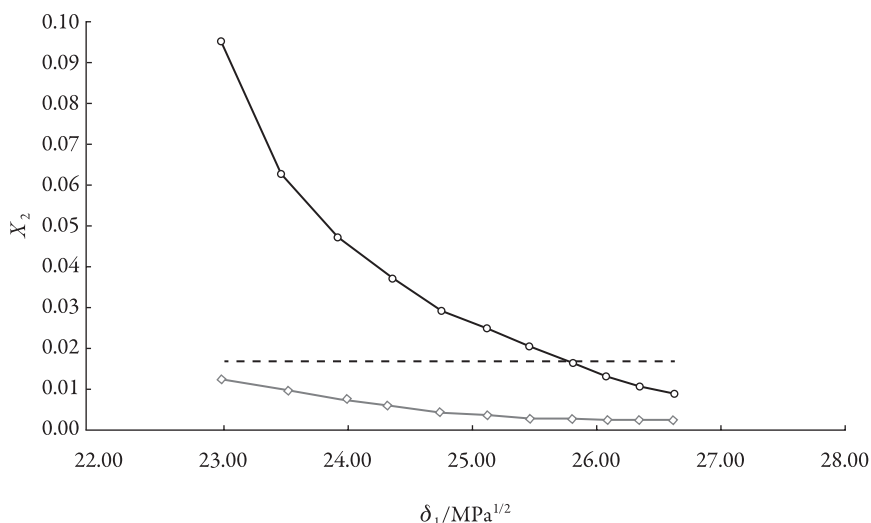


Figure 2. Experimental solubility (o) and calculated solubility according to the regular solutions model of Hildebrand ( $\diamond$ ) of nimodipine as a function of the solubility parameter of the solvent mixtures in PEG 400 + ethanol mixtures at 298.15 K. Discontinuous line is the ideal solubility of nimodipine.

Table 3.  $A$ ,  $K$ , and  $W$  experimental parameters for nimodipine in PEG 400 + ethanol mixtures at 298.15 K.

$\delta_1 / \text{MPa}^{1/2}$	$100 \times A / \text{cm}^3 \text{J}^{-1}$	$K / \text{J cm}^{-3a}$	$W_{\text{expt}} / \text{J cm}^{-3a}$
26.50	9.60369	0.507636	588.945
26.25	11.16058	0.507327	583.139
25.99	11.09398	0.506889	576.844
25.72	10.81196	0.506444	570.171
25.42	10.52472	0.506007	563.097
25.10	9.90281	0.505532	555.527
24.76	10.21916	0.504980	547.372
24.39	9.88033	0.504705	538.955
24.00	9.88260	0.504453	529.929
23.57	9.97447	0.504335	520.331
23.10	10.09080	0.504637	510.348

<sup>a</sup>  $1 \text{ J cm}^{-3} = 1 \text{ MPa}$ .

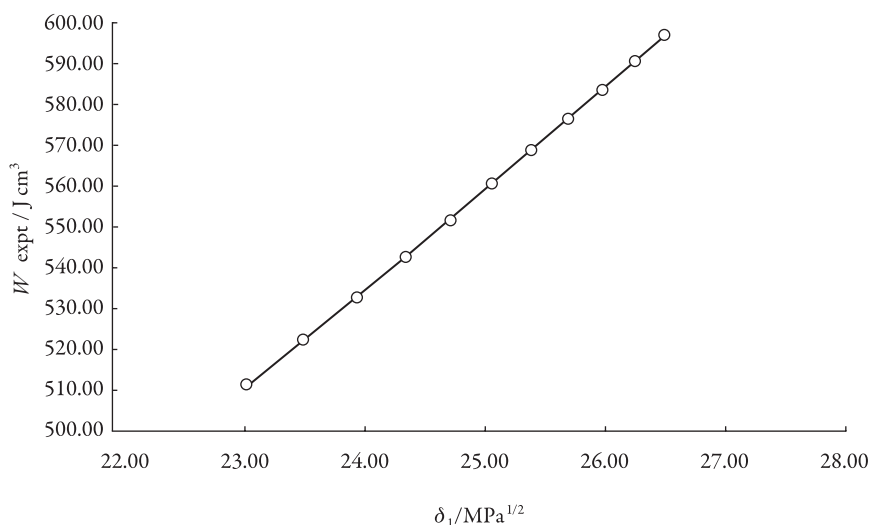


Figure 3.  $W$  parameter as a function of the solubility parameter of the solvent mixtures in PEG 400 + ethanol mixtures at 298.15 K.

$W$  values were adjusted to regular polynomials in orders from 2 to 5 (Equation 5). Nevertheless linear model was also evaluated with comparative purposes. Table 4 summarizes the coefficients obtained in all the regular polynomials from degrees one to five, whereas the  $W$  values calculated by using the respective polynomials are presented in Table 5. It is well clear that these values depend on the model used in the  $W$  back-calculation. Similar behaviors have been reported in the literature for this drug and for several other compounds in different solvent mixtures [16-38].

Table 6 summarizes the solubility values obtained by using the  $W$  values obtained by back-calculation from the polynomial models (Table 3) and presented in Table 4. In the same way as it was made previously [30-32, 34, 36-38] and because we are searching the best adjust, the first criterion used to define the polynomial order of  $W$  term as function of  $\delta_1$  was the fitting standard uncertainties obtained, whose values were as follows, 0.4926, 0.1333, 0.0464, 0.0468, and 0.0496 (Table 4), for orders one to five, respectively. So, the best one is obtained by using a polynomial in order 3. As another comparison criterion, Table 6 also summarizes the percentages of difference between NMD experimental solubility and those calculated by using EHSA.

Table 4. Coefficients and statistical parameters of regular polynomials in several orders of  $W$  as a function of solubility parameters of cosolvent mixtures free of nimodipine (Equation 5) in PEG 400 + ethanol mixtures. Values in parentheses are the respective uncertainties.

Coefficient or parameter	Polynomial order				
	1	2	3	4	5
$C_0$	-28 (3)	232 (24)	1,994 (229)	-4,231 (6,589)	118,653 (211,721)
$C_1$	23.25 (0.14)	2.3 (2.0)	-211 (28)	795 (1,064)	-24,020 (42,747)
$C_2$	-	0.42 (0.04)	9.0 (1.1)	-52 (64)	1,951 (3,450)
$C_3$	-	-	-0.116 (0.015)	1.5 (1.7)	-79 (139)
$C_4$	-	-	-	-1.7 (1.7) E-2	1.6 (2.8)
$C_5$	-	-	-	-	-1.3 (2.3) E-2
Adj. $r^2$	0.9996	1.0000	1.0000	1.0000	1.0000
Fit. Err.	0.4926	0.1333	0.0464	0.0468	0.0496

Table 5.  $W$  parameters ( $\text{J cm}^{-3a}$ ) back-calculated by using several polynomial models for nimodipine in PEG 400 + ethanol mixtures at 298.15 K.

$\delta_1 / \text{MPa}^{1/2}$	Polynomial order				
	1	2	3	4	5
26.50	588.461	589.133	588.972	588.956	588.818
26.25	582.759	583.112	583.100	583.111	582.992
25.99	576.692	576.762	576.844	576.861	576.738
25.72	570.225	570.057	570.177	570.188	570.053
25.42	563.316	562.965	563.074	563.073	562.931
25.10	555.919	555.456	555.510	555.498	555.359
24.76	547.980	547.490	547.466	547.451	547.322
24.39	539.437	539.030	538.925	538.919	538.798
24.00	530.219	530.027	529.883	529.894	529.767
23.57	520.242	520.434	520.347	520.369	520.224
23.10	509.408	510.193	510.351	510.339	510.214

<sup>a</sup>  $1 \text{ J cm}^{-3} = 1 \text{ MPa}$ .

Table 6. Calculated solubility of nimodipine in PEG 400 + ethanol mixtures by using the  $W$  parameters obtained from regression models in orders 1, 2, 3, 4 and 5, and difference percentages with respect to the experimental values at 298.15 K.

$\delta_1$ (MPa <sup>1/2</sup> )	$X_2$ calculated					% dev. <sup>a</sup>				
	1	2	3	4	5	1	2	3	4	5
26.50	5.59 E-3	7.53 E-3	7.01 E-3	6.96 E-3	6.55 E-3	19.3	8.7	1.2	0.5	5.5
26.25	7.06 E-3	8.47 E-3	8.42 E-3	8.46 E-3	7.96 E-3	17.7	1.4	1.9	1.4	7.3
25.99	1.04 E-2	1.08 E-2	1.12 E-2	1.13 E-2	1.07 E-2	7.5	4.1	0.0	0.9	5.3
25.72	1.51 E-2	1.39 E-2	1.47 E-2	1.48 E-2	1.38 E-2	2.7	5.5	0.3	0.9	5.7
25.42	2.10 E-2	1.77 E-2	1.87 E-2	1.87 E-2	1.74 E-2	11.2	6.2	1.1	1.2	7.7
25.10	2.76 E-2	2.23 E-2	2.29 E-2	2.28 E-2	2.14 E-2	19.6	3.2	0.8	1.3	7.4
24.76	3.69 E-2	2.93 E-2	2.89 E-2	2.87 E-2	2.70 E-2	33.1	5.7	4.5	3.8	2.3
24.39	4.46 E-2	3.71 E-2	3.54 E-2	3.53 E-2	3.34 E-2	24.5	3.4	1.4	1.6	6.9
24.00	5.29 E-2	4.85 E-2	4.54 E-2	4.57 E-2	4.31 E-2	14.1	4.6	2.1	1.6	7.1
23.57	5.95 E-2	6.49 E-2	6.24 E-2	6.30 E-2	5.90 E-2	4.0	4.8	0.7	1.7	4.8
23.10	6.15 E-2	8.85 E-2	9.53 E-2	9.48 E-2	8.94 E-2	35.4	7.0	0.1	0.5	6.1
Mean value <sup>b</sup>						17.2	5.0	1.3	1.4	6.0
Standard deviation <sup>b</sup>						10.8	2.0	1.3	0.9	1.6

<sup>a</sup> Calculated as  $100 \times |X_2 \text{ expt} - X_2 \text{ calc}| / X_2 \text{ expt}$ .

<sup>b</sup> Calculated considering the obtained values in the neat solvents and the nine binary mixtures.

At the beginning, it is found that as more complex the polynomial used is, better the agreement found between experimental and calculated solubility is, reaching the maximum concordance using a polynomial in order three. This result is different way to those reported in the literature for other pharmaceutical compounds where the concordance always increases with the polynomial degree [16-38]. Most important increment in concordance is obtained passing from order 1 to order 2, but the more significant increment is also obtained from order 2 to order 3. Therefore, in the following comparisons the polynomial model in order 3 is used.

As has been exposed previously, an important consideration about the usefulness of the EHSA method is the one referent to justify the complex calculations involving any other variables, instead of the simple empiric regression of the experimental solubility as a function of the solvent mixtures' solubility parameters (Table 1, Figure 4). For this reason, in the Table 7 the experimental solubilities are confronted to those cal-

culated directly by using a regular polynomial in order 3 of  $\log X_2$  as a function of  $\delta_1$  values (Equation 8, with adjusted determination coefficient  $r^2 = 0.9989$  and fitting standard uncertainty = 0.0108) and also to those calculated involving the  $W$  parameters obtained from equation 5 adjusted to order 3 (Tables 4 and 5). The respective difference percentages are also presented in Table 7.

$$\log X_2 = 344(\pm 54) - 42(\pm 6)\delta_1 + 1.68(\pm 0.26)\delta_1^2 - 2.3(\pm 0.4) \times 10^{-2} \delta_1^3 \quad (\text{Eq. 8})$$

Table 7. Comparison of the nimodipine solubility values in PEG 400 + ethanol mixtures calculated directly and by using the EHSA at 298.15 K.

$\delta_1 / \text{MPa}^{1/2}$	$X_2$			% dev. <sup>a</sup>	
	Exptl.	Calc. direct. <sup>b</sup>	Calc. $W^c$	Calc. direct.	Calc. $W$
26.50	6.93 E-3	6.75 E-3	7.01 E-3	2.6	1.2
26.25	8.58 E-3	8.88 E-3	8.42 E-3	3.4	1.9
25.99	1.12 E-2	1.15 E-2	1.12 E-2	2.1	0.0
25.72	1.47 E-2	1.46 E-2	1.47 E-2	0.3	0.3
25.42	1.89 E-2	1.84 E-2	1.87 E-2	2.9	1.1
25.10	2.31 E-2	2.29 E-2	2.29 E-2	1.0	0.8
24.76	2.77 E-2	2.84 E-2	2.89 E-2	2.6	4.5
24.39	3.59 E-2	3.57 E-2	3.54 E-2	0.5	1.4
24.00	4.64 E-2	4.61 E-2	4.54 E-2	0.7	2.1
23.57	6.19 E-2	6.29 E-2	6.24 E-2	1.6	0.7
23.10	9.52 E-2	9.46 E-2	9.53 E-2	0.6	0.1
		Mean value <sup>d</sup>		1.7	1.3
		Standard deviation <sup>d</sup>		1.1	1.3

<sup>a</sup> Calculated as  $100 \times |X_2 \text{ expt} - X_2 \text{ calc}| / X_2 \text{ expt}$ .

<sup>b</sup> Calculated using the equation 8.

<sup>c</sup> Calculated using the equation 5 adjusted to order 3 (Tables 4 and 5).

<sup>d</sup> Calculated considering the obtained values in the neat solvents and the nine binary mixtures.

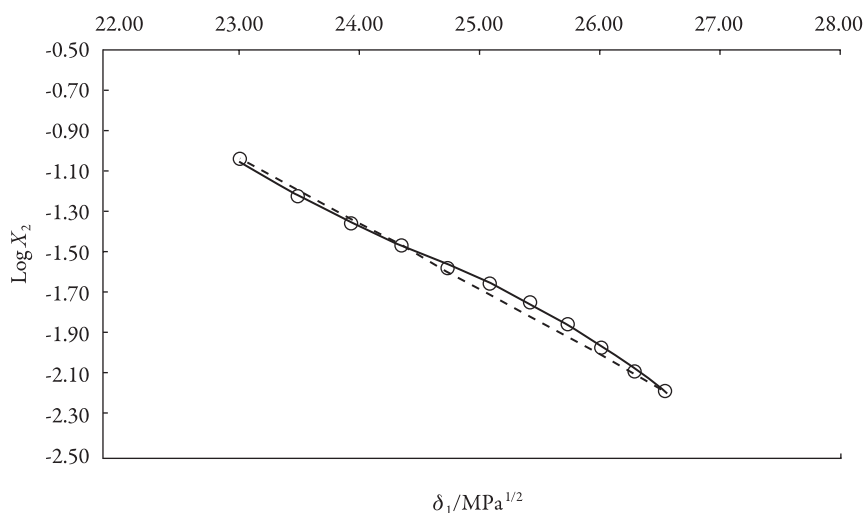


Figure 4. Logarithmic solubility of nimodipine as a function of the solubility parameter of the solvent mixtures in PEG 400 + ethanol mixtures at 298.15 K. Dotted line is the additive solubility behavior.

Based on mean deviation percentages presented in Table 7 (1.7% and 1.3% for direct calculation and EHSA method, respectively) it follows that a small difference is found between the values obtained by using both methods. The present results would be showing a significant usefulness of EHSA method for practical purposes.

On the other hand, it is very interesting to note that this drug exhibit negative and positive deviations with respect to ideal log-linear additive model (dotted line in Figure 4). Nevertheless the molecular reasons for this behavior are unclear due to the lack of information about structural effects in these binary mixtures [47, 48].

## CONCLUSION

In this investigation the ehSA method has been adequately used to study the solubility of nmd in PEG 400 + ethanol mixtures by using experimental values of molar volume and calculated Hildebrand solubility parameter of this drug. In particular, a good predictive character has been found by using a regular polynomial in order three of the interaction parameter  $W$  as a function of the solubility parameter of solvent mixtures free of solute. This result is different to that reported for other pharmaceutical compounds in terms of polynomial order and fitting obtained. Nevertheless, the predictive character is just slightly better than the one obtained by direct correlation between solubility and mixtures composition.

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